

Amendments to the Claims:

This listing of claims replaces all prior versions and listings of claims in the application:

Listing of Claims:

1. (Original) A chemically defined medium for fermentation culture of a strain of the genus *Candida*, which comprises 1-10 g/l of urea, 1-10 g/l of potassium diphosphate, 0.01-1 g/l of magnesium sulfate, 0.1-10 mg/l of  $\text{MnSO}_4 \cdot 4\text{H}_2\text{O}$ , 0.1-10 mg/l of  $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$ , 0.1-10 mg/l of  $\text{NaMoO}_4 \cdot 2\text{H}_2\text{O}$ , 0.1-10 mg/l of  $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$ , 0.1-10 mg/l of  $\text{AlCl}_3 \cdot 6\text{H}_2\text{O}$ , 0.1-10 mg/l of  $\text{CuCl}_2 \cdot 2\text{H}_2\text{O}$ , 0.01-5 mg/l of  $\text{H}_3\text{BO}_3$ , 1-100 mg/l of  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ , 0.1-10 mg/l of ascorbic acid, 1-100 mg/l of biotin, 1-100 mg/l of choline, and 0.1-10 mg/l of pyridoxine.

2. (Original) A process for producing xylitol in high yield by recycling culture of a strain of the genus *Candida*, which comprises the steps of :

inoculating the strain in a xylose-containing medium and culturing the strain in the xylose-containing medium in a bioreactor;

releasing a culture from the bioreactor and introducing a fresh xylose-containing medium to the bioreactor continuously;

separating the strain and a culture filtrate from the culture; and

recycling the strain to the bioreactor and recovering xylitol from the culture filtrate.

3. (Original) The process of claim 2, wherein the strain of the genus *Candida* is *Candida tropicalis* or its mutant strain.

4. (Currently Amended) The process of claim 2, wherein the xylose-containing medium is ~~[[the]]~~ a chemically defined medium ~~of claim 1~~ that comprises 1-10 g/l of urea, 1-10 g/l of potassium diphosphate, 0.01-1 g/l of magnesium sulfate, 0.1-10 mg/l of  $\text{MnSO}_4 \cdot 4\text{H}_2\text{O}$ , 0.1-10 mg/l of  $\text{CoCl}_2 \cdot 6\text{H}_2\text{O}$ , 0.1-10 mg/l of  $\text{NaMoO}_4 \cdot 2\text{H}_2\text{O}$ , 0.1-10 mg/l of  $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$ , 0.1-10 mg/l of  $\text{AlCl}_3 \cdot 6\text{H}_2\text{O}$ , 0.1-10 mg/l of  $\text{CuCl}_2 \cdot 2\text{H}_2\text{O}$ , 0.01-5 mg/l of  $\text{H}_3\text{BO}_3$ , 1-100 mg/l of  $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ , 0.1-10 mg/l of ascorbic acid, 1-100 mg/l of biotin, 1-100 mg/l of choline, and 0.1-10 mg/l of pyridoxine; or a complex medium.

5. (Original) The process of claim 2, wherein the culturing is performed by a fed-batch culture or a batch culture.

6. (Original) The process of claim 5, wherein in the fed-batch culture, the medium is gradually supplemented with xylose so that the concentration of xylose is maintained at 40-50 g/l on the basis of the medium.

7. (Currently Amended) The process of ~~any one of claims 2, 4, 5, and 6~~ claim 2, wherein the culturing is performed at an agitation speed of 400-600 rpm.

8. (Original) The process of claim 2, wherein the separation of the strain and the culture filtrate from the culture is performed by a vacuum microfiltration system or a centrifuge.

9. (Currently Amended) The process of claim 2 ~~[[ or 8]]~~, wherein the separated strain is concentrated to a density of 10-100 g/l and recycled.

10. (New) The process of claim 4, wherein the culturing is performed at an agitation speed of 400-600 rpm.

11. (New) The process of claim 5, wherein the culturing is performed at an agitation speed of 400-600 rpm.

12. (New) The process of claim 6, wherein the culturing is performed at an agitation speed of 400-600 rpm.

13. (New) The process of claim 8, wherein the separated strain is concentrated to a density of 10-100 g/l and recycled.